

Sulfate Reducing Bioreactor Engineering Principles

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Passive Treatment System Design Components

Biological Components

- **Anaerobic SRBR's**
- Aerobic Cells or Rock Filters
- Successive Alkalinity Producing Systems (SAPS)

Limestone Components

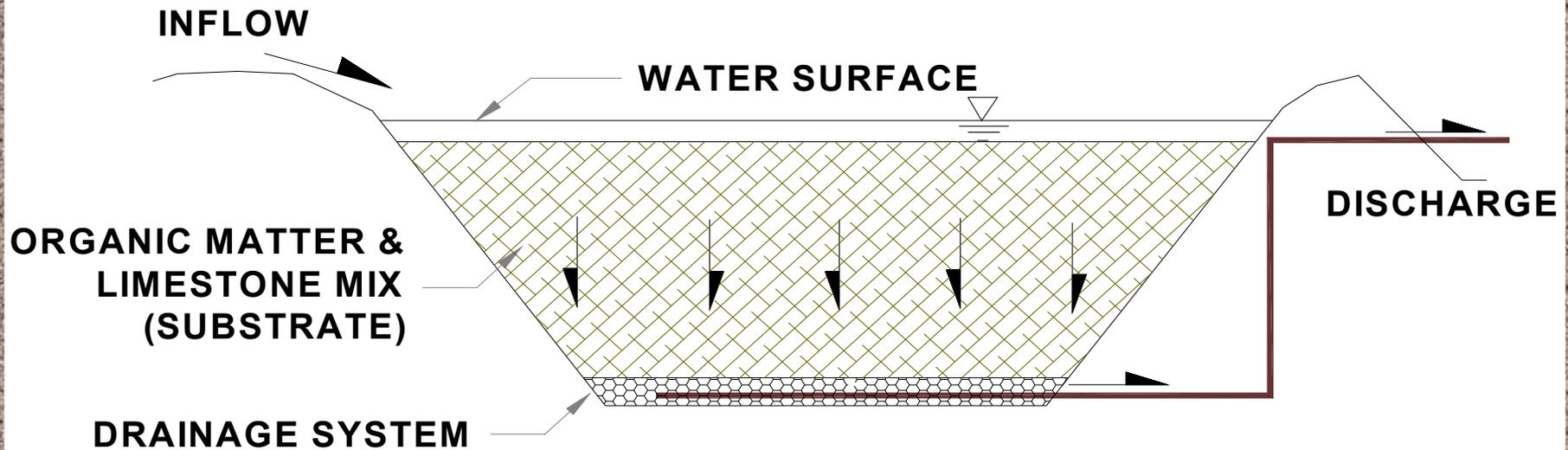
- Limestone Sand
- Anoxic Limestone Drains (ALD's)
- Alkaline Ponds
- Open Limestone Channels

Settling Ponds & Flow Equalization Ponds,
Fluid Conveyances (Pipes & Channels)

Rocket Science?



Sulfate Reducing Bacteria Cell Schematic Cross Section



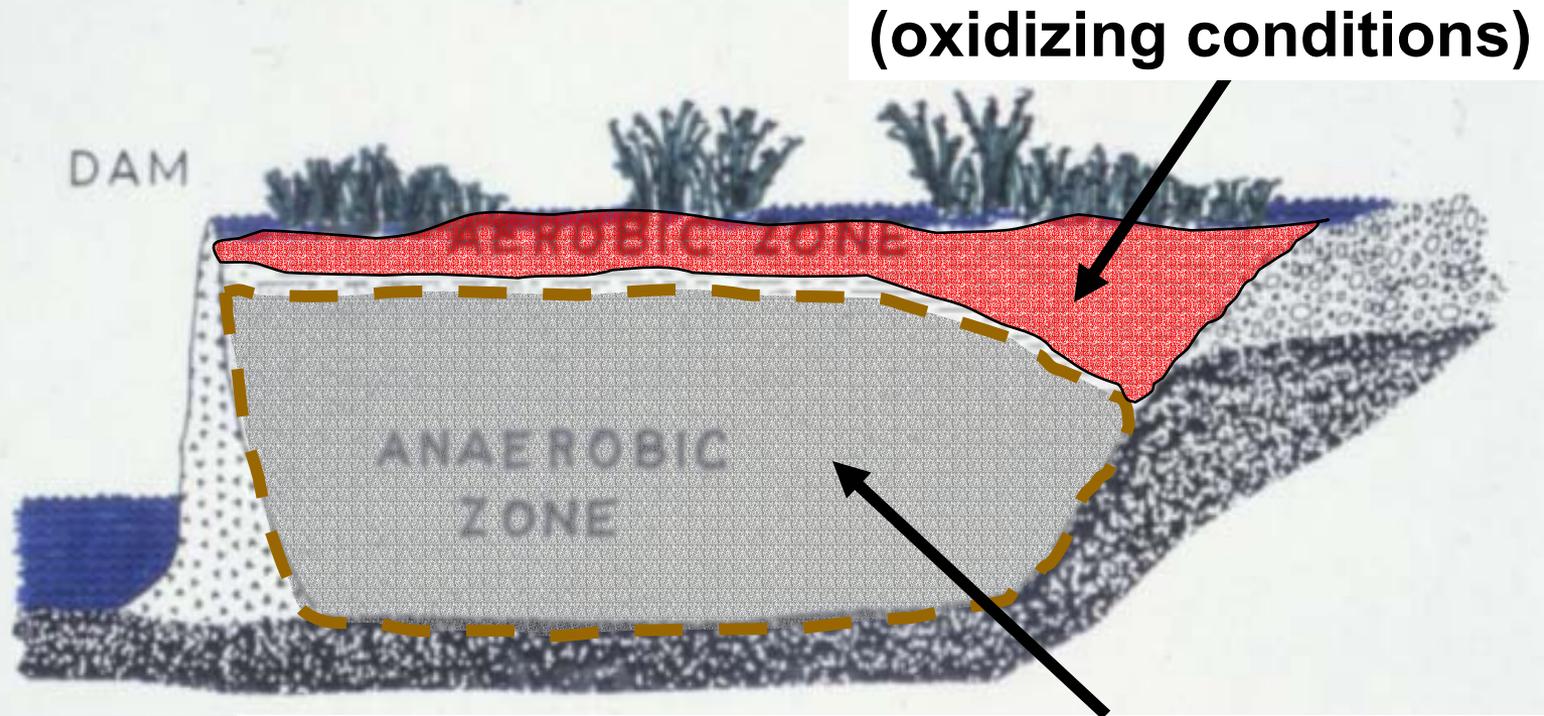
Anaerobic SRBR's

AKA Vertical
Flow Reactors

Aluminum and
heavy metal
removal, pH
adjustment,
alkalinity addition



Typical Wetland Ecosystem



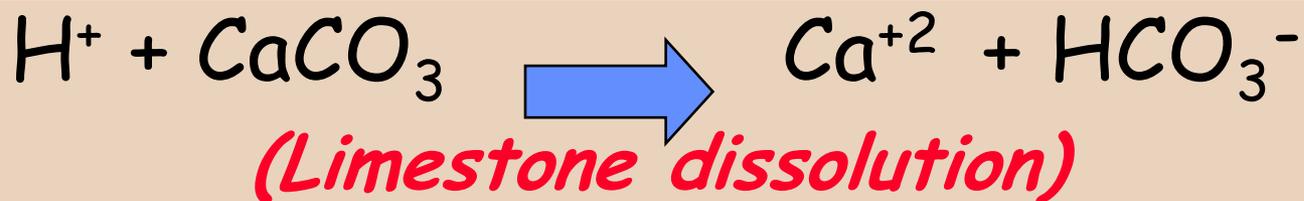
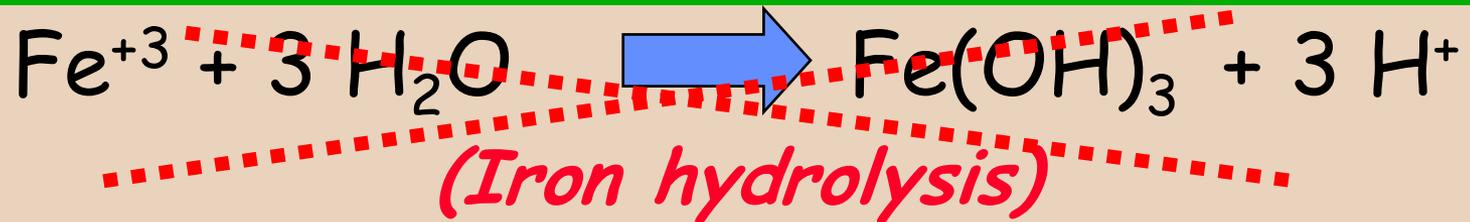
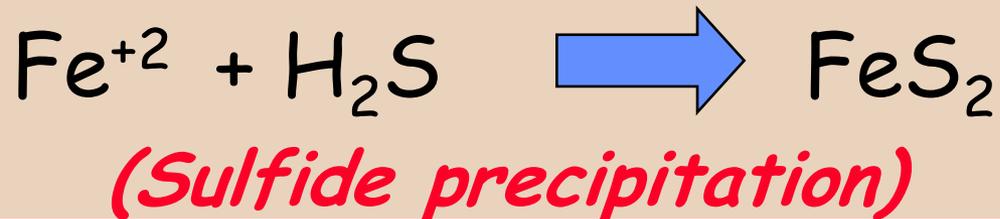
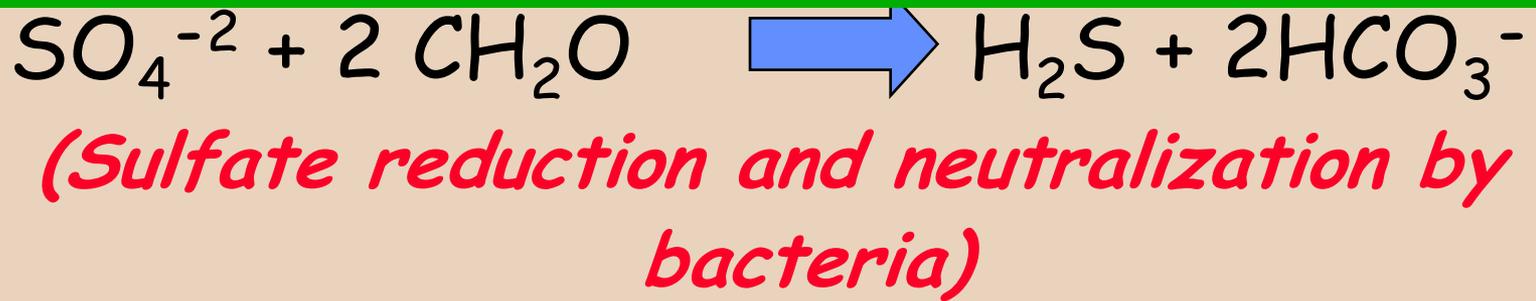
(oxidizing conditions)

Sulfate Reducing Bacteria (SRB's)
live here (reducing conditions)



Oxidation and Reduction Processes in Competition

SRBR Chemistry 101



SRBR Chemistry 102

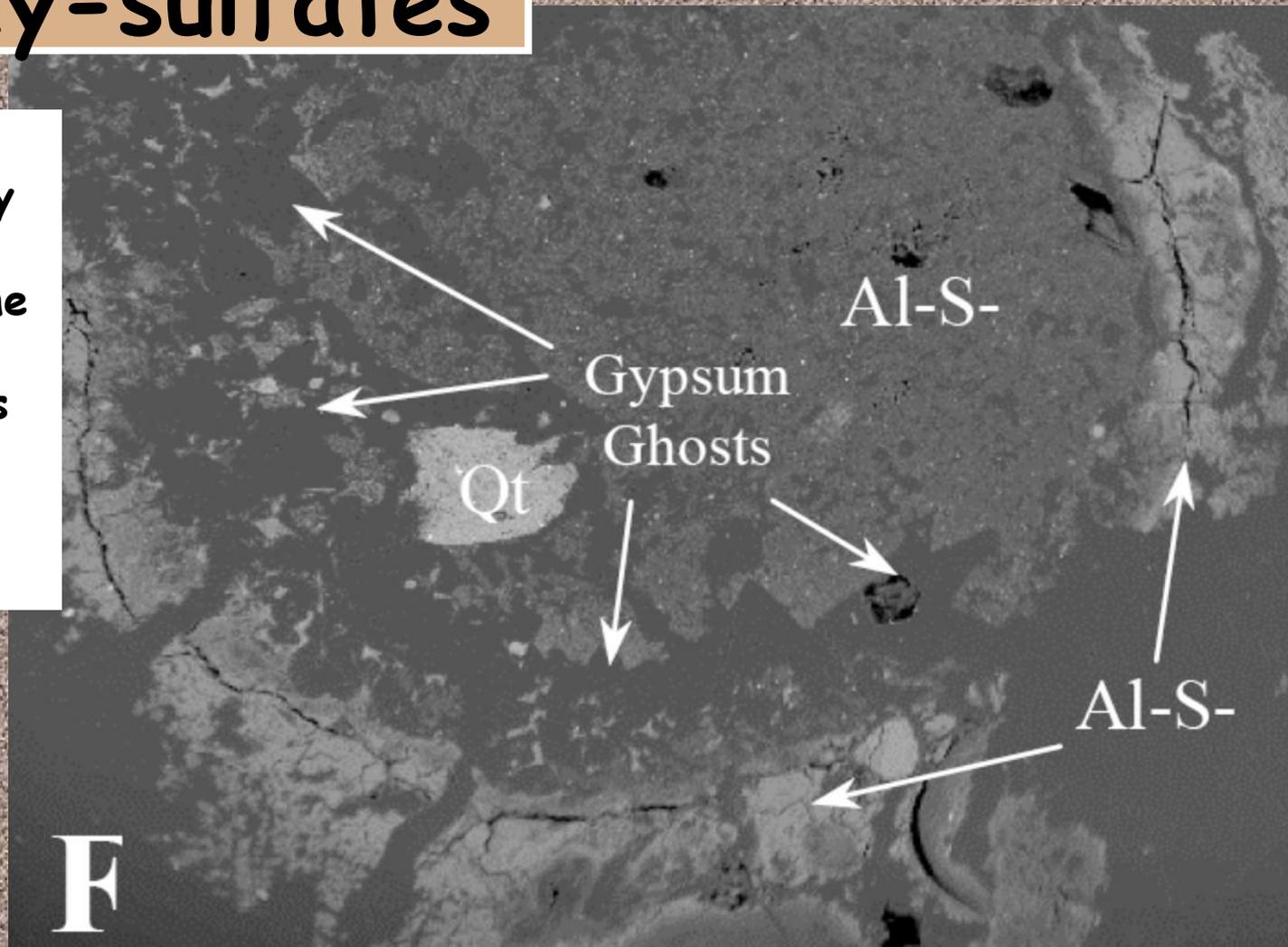
Aluminum Precipitation Reactions



There are **at least** another 123 possible reactions.

Aluminum Hydroxy-sulfates

Limestone ghost outlined and partially filled by aluminum hydroxy-sulfate. The former presence of blocky gypsum grains is preserved by the later aluminum hydroxy-sulfate.



200µm
BEI 44A-3a

Ref: B. T. Thomas, 2002

SRBR Chemistry 103

Selenium Removal Reactions

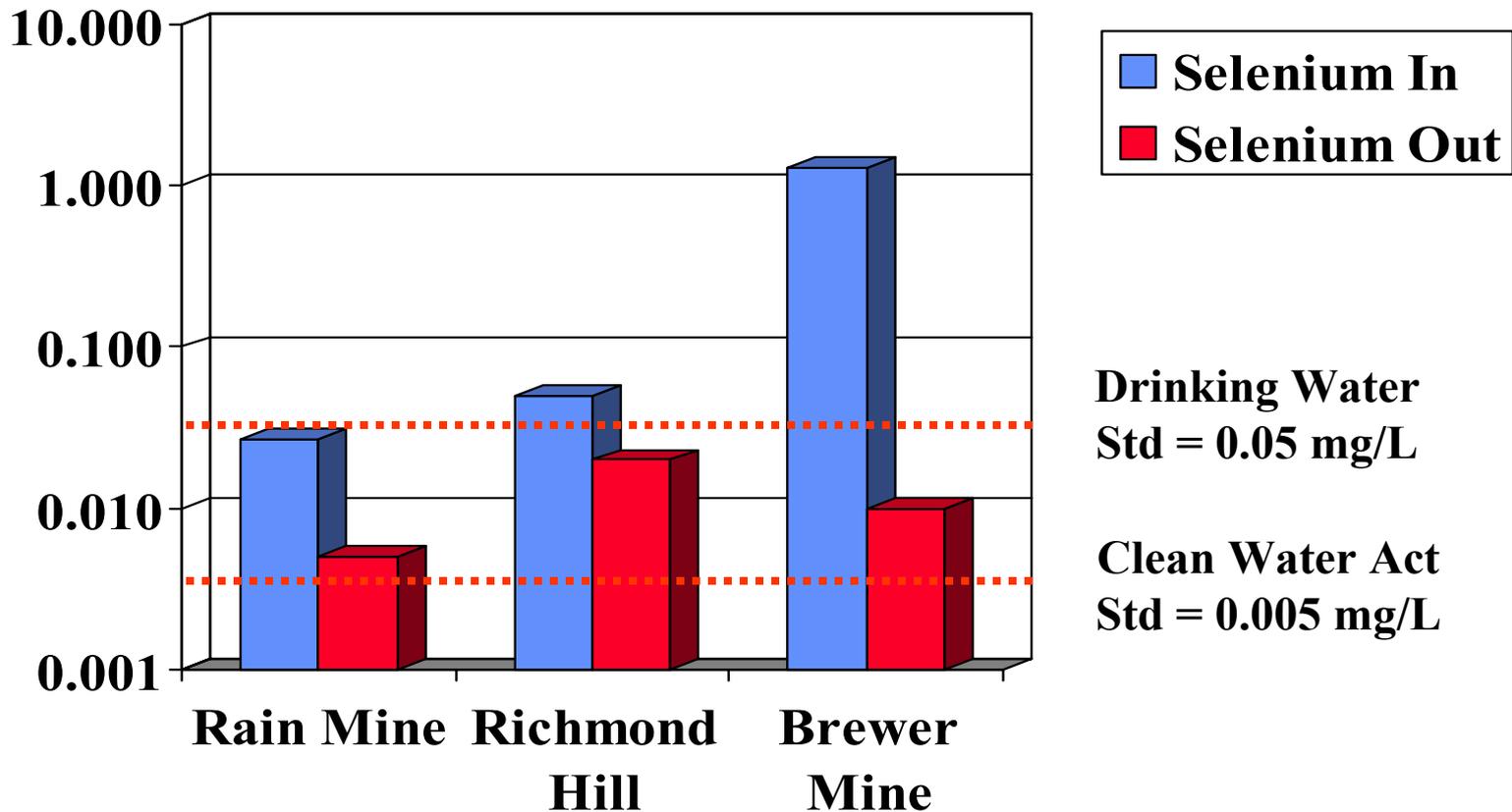
Reduction / Precipitation

Se^{6+} and $\text{Fe}^{2+} \Rightarrow \text{Se}^{4+}$ and Fe^{3+} (or other reductant)

$3\text{Se}^{4+} + 2\text{Fe}(\text{OH})_2 + 8\text{H}_2\text{O} + 1/2\text{O}_2 \Rightarrow \text{Fe}_2(\text{SeO}_3)_3 \bullet 4\text{H}_2\text{O} + 12\text{H}^+$
(amorphous ferric selenite)

$\text{Se}^{6+} + \text{bacteria (} P. \text{ stutzeri)} + \text{nutrients} \Rightarrow \text{Se (elemental selenium)}$ This process may be restricted to Se concentrations greater than about 10 ppb due to bacterial "starvation".

Secondary Selenium Passive Treatment



SRBR Chemistry 104

Arsenic Removal

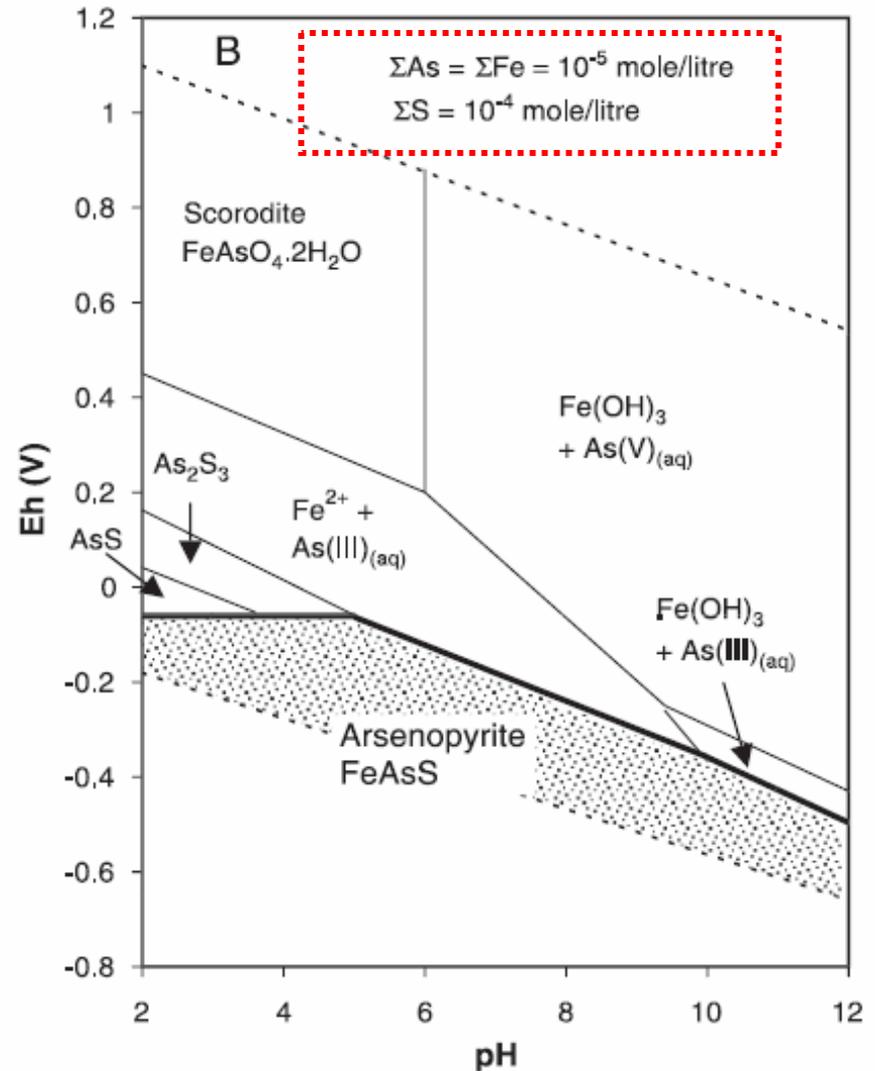
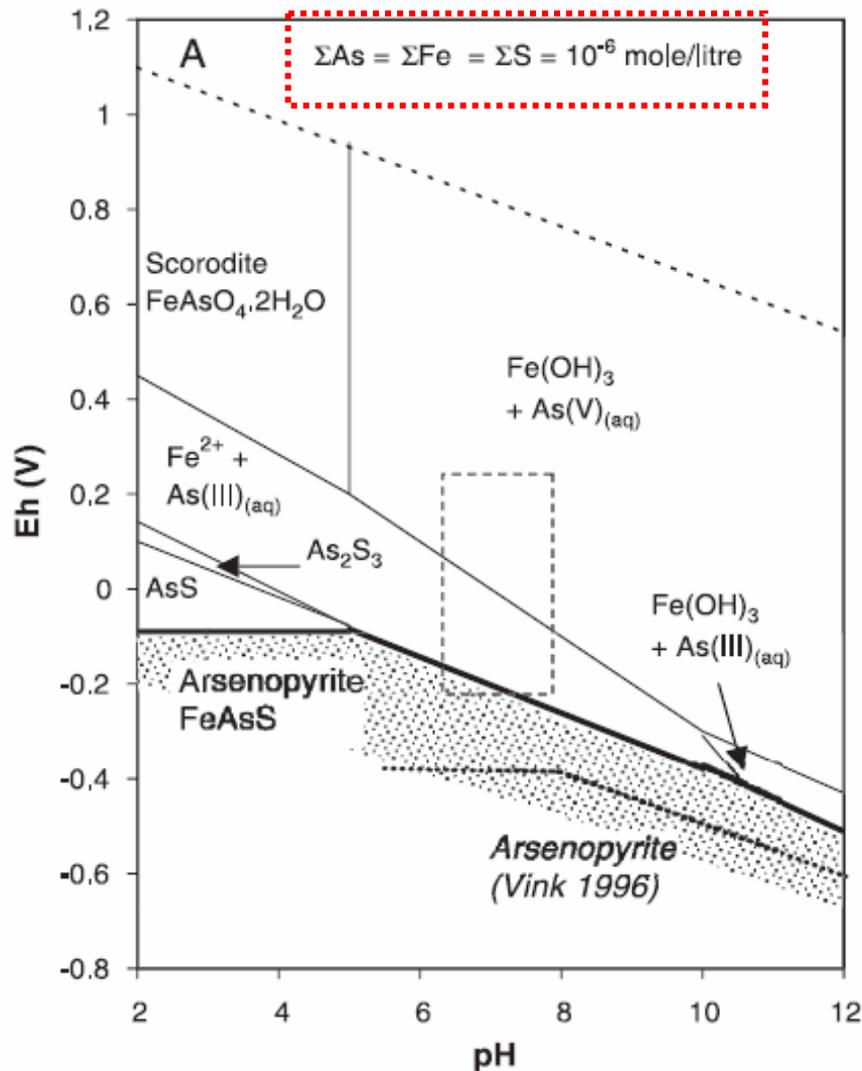
Removal as a sulfide either as

ORPIMENT (As_2S_3),

or *REALGAR* (AsS)

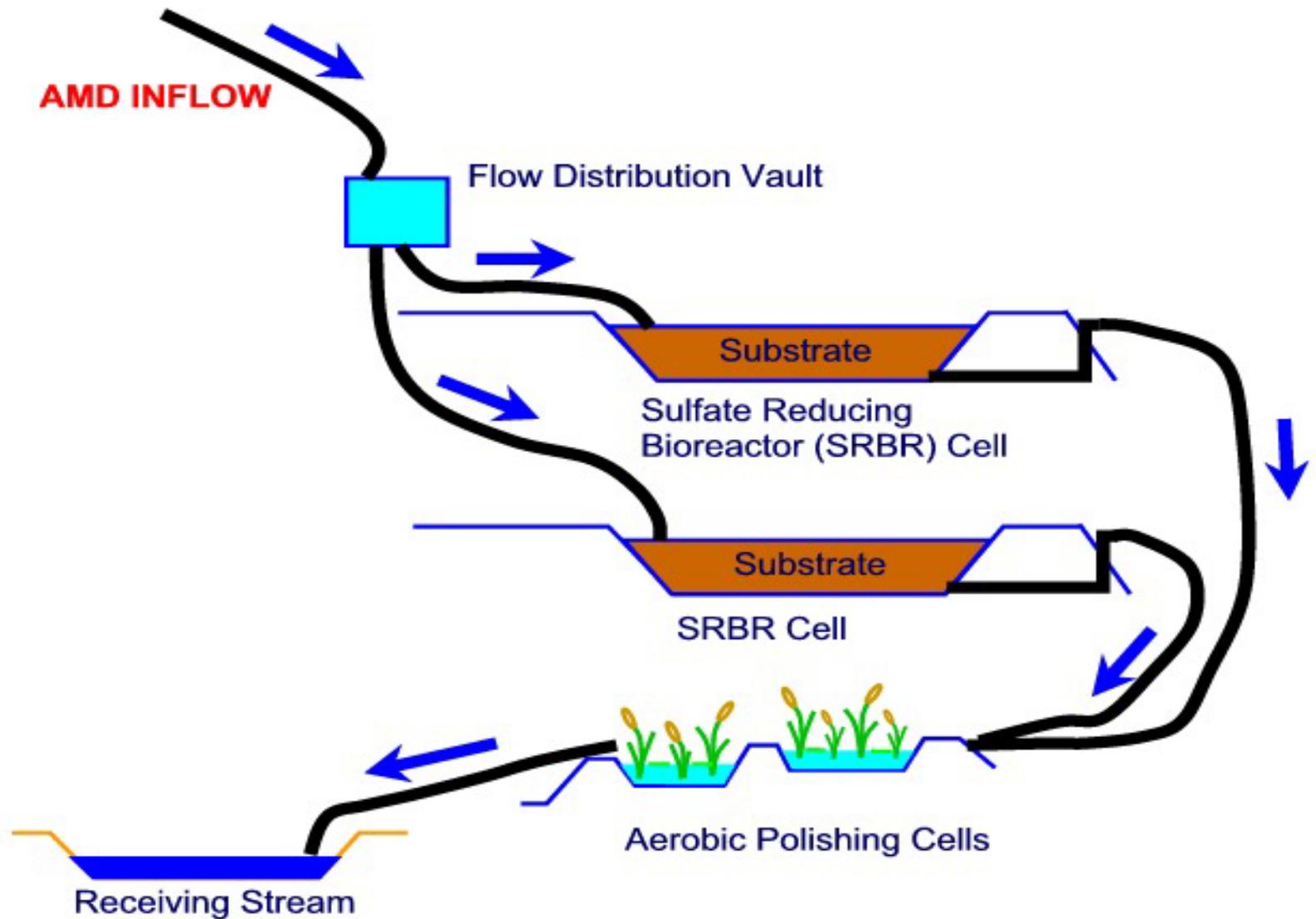
or *ARSENOPYRITE* ($FeAsS$)

pH-Eh Diagrams Arsenic



(A) Diagram calculated for dissolved As, Fe, and S of 10^{-6} mol/l.

(B) Diagram calculated for dissolved As and Fe of 10^{-5} mol/l and S of 10^{-4} mol/l.

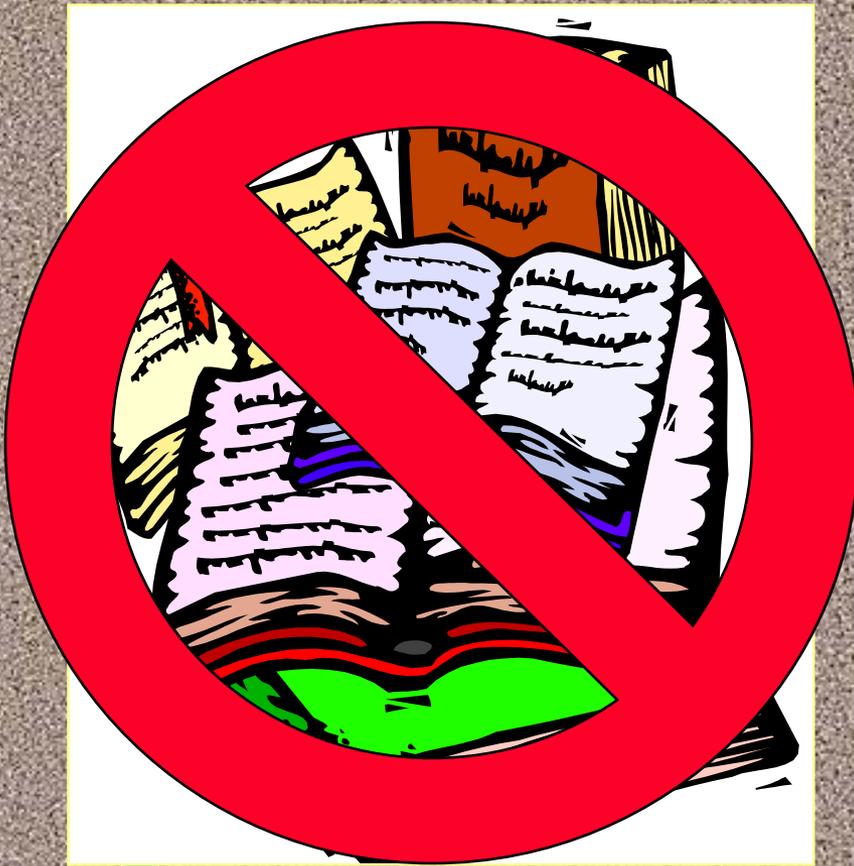


Passive Treatment System Containment Structures

- Natural soil-lined excavation
- Geomembrane-lined excavation
- Structural concrete (OK for pilot systems)
- Pre-fabricated metal/fiberglass tanks (OK for pilot systems)
- Other (rock excavations -underground?)

SRBR Design Parameters

NO COOKBOOK (YET)



- ARD Geochemistry (cell sequencing & cell type)
- Metal Loading = (concentration X flow rate)
- Surface Area is a function of loading
- Cell Depth is a function of loading

Metal Loading

Metal Loading = (concentration X flow rate)

20 mg Fe/Liter x **8 gal/min** x 3.785 L/gal x
1 gram/1000 mg x 1,440 min/day =

872 grams Fe per day = 15.6 moles/day

**1 mole of Fe weighs 55.85 grams
one mole of sulfate (96 grams) is consumed
for every mole of iron**

- **Darcy's Law** is satisfied, slight ponding on the surface of SRBR cells (to discourage emergent plants and distribute flow evenly)
- **Area Loading Factor/Flux** may vary with pH or mineral acidity; USBM recommended 50 grams acidity/day/m² as a starting point *(may not be conservative enough)*
- **Rule of Thumb: Precipitated Metal Mass Loading** - 0.3 moles of metal per cubic meter of cell volume per day (function of substrate "roughage" characteristics)
- **Sulfate Reducing Stoichiometry** - carbon/organic and alkalinity content of substrate mass are most likely limiting factors on substrate longevity



Design Methods I - SRBR Cells

- **Precipitated Metal Volumetric Loading** - filling of substrate void spaces with precipitates (not limiting)
- **Self-Sustaining Capability** - dying plants replenish substrate to provide void spaces and more organic material
- **Water Balance** - evapotranspiration effects
- **Surface and Ground Water Hydrology** - protect system from the design storm and consider local ground water conditions

Design Methods II - SRBR Cells

DARCY'S LAW

$$Q = k \times i \times A$$

Where:

Q is flow, cubic centimeters/second

k is permeability of material,
centimeters per second

i is the hydraulic gradient, unitless, but it is also the pressure loss,
dH, over the depth of the substrate material, L;

$$\text{i.e.,} = \frac{\text{dH (cm)}}{\text{L (cm)}} = i$$

A is the cross sectional area of the SRBR perpendicular to the flow
path

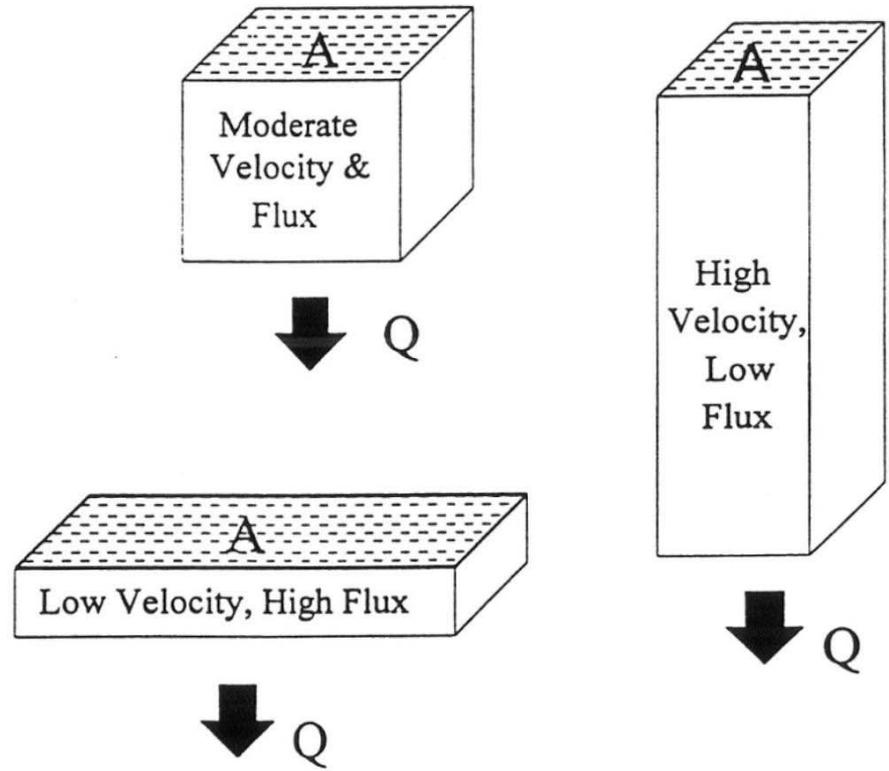
FLUX = Q/A = FLOW/AREA (velocity)

Area Loading Factor/ Flux What does it mean?

$$\frac{1}{\text{DARCY FLUX}} = \frac{\text{Area}}{\text{Flow}} \approx 0.25 \text{ to } 500 \text{ sq m per Liter/min}$$

Area Loading Factor ✓

The higher the acidity, the higher the flux value/area loading factor



SRBR Cell Design Parameters I

- 0.3 moles of sulfate reduction per cubic meter per day (volumetric load)
- Organic Substrate that's permeable
- Organic Substrate with alk. source
- 10 to over 2000 ft²/gpm (function of AMD mineral acidity)**

*** The better the water, the smaller the footprint*

Substrate Selection

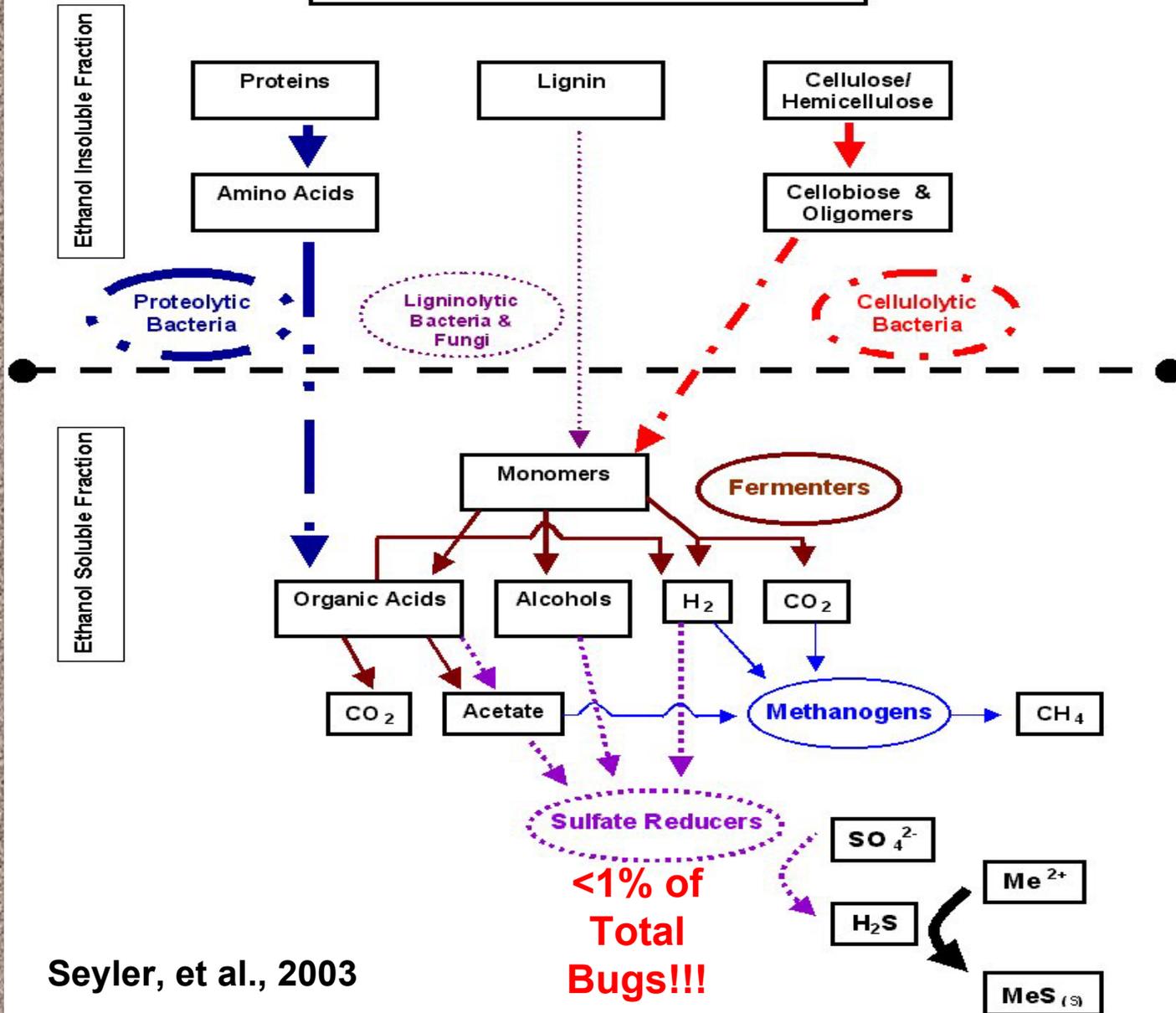
Chemical Characteristics

- Net Alkaline (this can be added limestone)
- SRBR Anaerobic Microbe Suite Source
- Low in Nitrogen
- Sulfate Reduction Potential is greater than the Anaerobic Fermentation Potential
- Check Methanogenesis Potential
$$2 \text{CH}_2\text{O} \rightarrow \text{CH}_4 + \text{CO}_2$$
- Electrical conductivity of substrate is roughly equal to the conductivity of AMD
- (New) measurement of Ethanol Soluble and Non-Soluble fractions targeting Cellulose/Cellobiose
- Variety of organic types to assist in startup but sustain long-term performance

Organic Substrate Degradation

- Wood chips
- Sawdust
- Rice hulls
- Yard waste
- Mushroom compost
- Animal manure
- Hay and straw (spoiled)
- Nut shells
- Cardboard
- Soy bean hulls
- Waste alcohols including antifreeze
- Waste dairy products
- Sugar cane processing residue (Bagasse)
- Rice straw
- Cotton waste

Conceptual Microbial Process Model



Seyler, et al., 2003

Sulfate Reducing Bacteria Suite Sources

**MUSHROOM COMPOST CAN ALSO USED
AS AN SRBR INOCULUM SOURCE**

Inorganic Material Sources

- Limestone
- Dolomitic Limestone?
- Cement Kiln Dust or Clinker
- Zero Valent Iron (ZVI)
- Steel Slag
- Other alkalinity generating wastes
- Inert drainage rock

Substrate Physical Parameters

- Saturated Hydraulic Conductivity (permeability) - tough to measure with bacterial activity
- Material Classification (size distribution & carbon content)
- Moisture-density/compaction relationships (can you drive equipment on it?)
- Porosity/void ratio (needed to estimate retention times)
- Specific gravity of solids (est. mass depletion rates)
- "Shrinkage" factors (what happens when two dissimilar solids are mixed?)
- Bulk Density of mix (how much volume and/or tonnage is needed to build the cell?)

Passive Treatment Staged Design Phases

- Lab (proof of principle) tests
- Bench tests
- Pilot tests
- Limited full scale (modules)
- Full scale implementation

Passive Treatment Lab - Proof of Principle Tests

Buckeye Landfill,
OH
POP Test Bottles



Brewer Gold Mine, SC
POP Test Bottles



Passive Treatment Bench Scale Tests



**Weekly sampling
schedule is typical**

Bench SRB Biopsy



Bench Test Biopsy



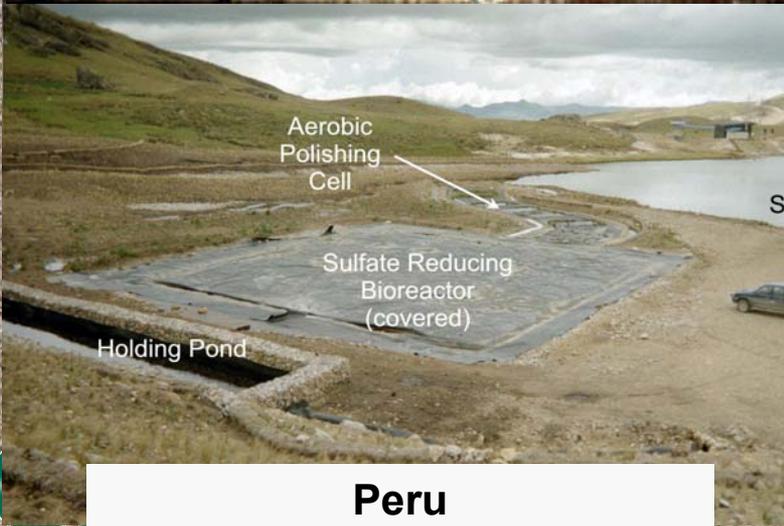
SRBR Pilot Scale Cells



Wyoming



Missouri



Peru



Pennsylvania

Operation and Maintenance Considerations I

Stresses On Organic Substrate:

- Precipitation of metals in void spaces (*this is somewhat counter-balanced by substrate dissolution*)
- Consumption of organic matter/carbon
- Consumption of alkalinity (especially with aluminum in AMD)
- Loss of permeability from compaction, settlement or humification

Operation and Maintenance Considerations II

System Stresses:

- Sub-freezing conditions
- Precipitate plugging valves and pipes
- Burrowing animals
- Storm event damage and drought (bypass extraordinary high flows and mix with net alkaline SRBR effluent)

Operation and Maintenance Considerations III

How do you measure SRBR performance?

- pH (if low, it had better go up and if neutral, it shouldn't change)
- Conductivity (minor increase expected after break-in)
- Calcium *in* vs Calcium *out* (limestone depletion)
- Sulfate *in* vs Sulfate *out* (estimate organic depletion)
- Oxidation Reduction Potential (less than -100 millivolts in effluent indicative of reducing conditions)
- Manganese unchanged
- 99%+ removal of all metals
- Alkalinity increase to about 300 mg/L
- After break in period, if Mn increases or effluent metals are greater than influent metals, SRBR is likely overloaded.

Major Overhaul & Maintenance Considerations in Design

- Removal of existing substrate materials
Removal of some aspects of cell plumbing/water distribution system
- Protection of liners
- Substrate processing for metal removal?
- New substrate purchase & installation
- Replanting vegetation (aerobic polishing)
- Temporary treatment of effluent during overhaul (parallel systems or holding pond)

Why Don't SRBR/Passive Systems Always Work As Designed?

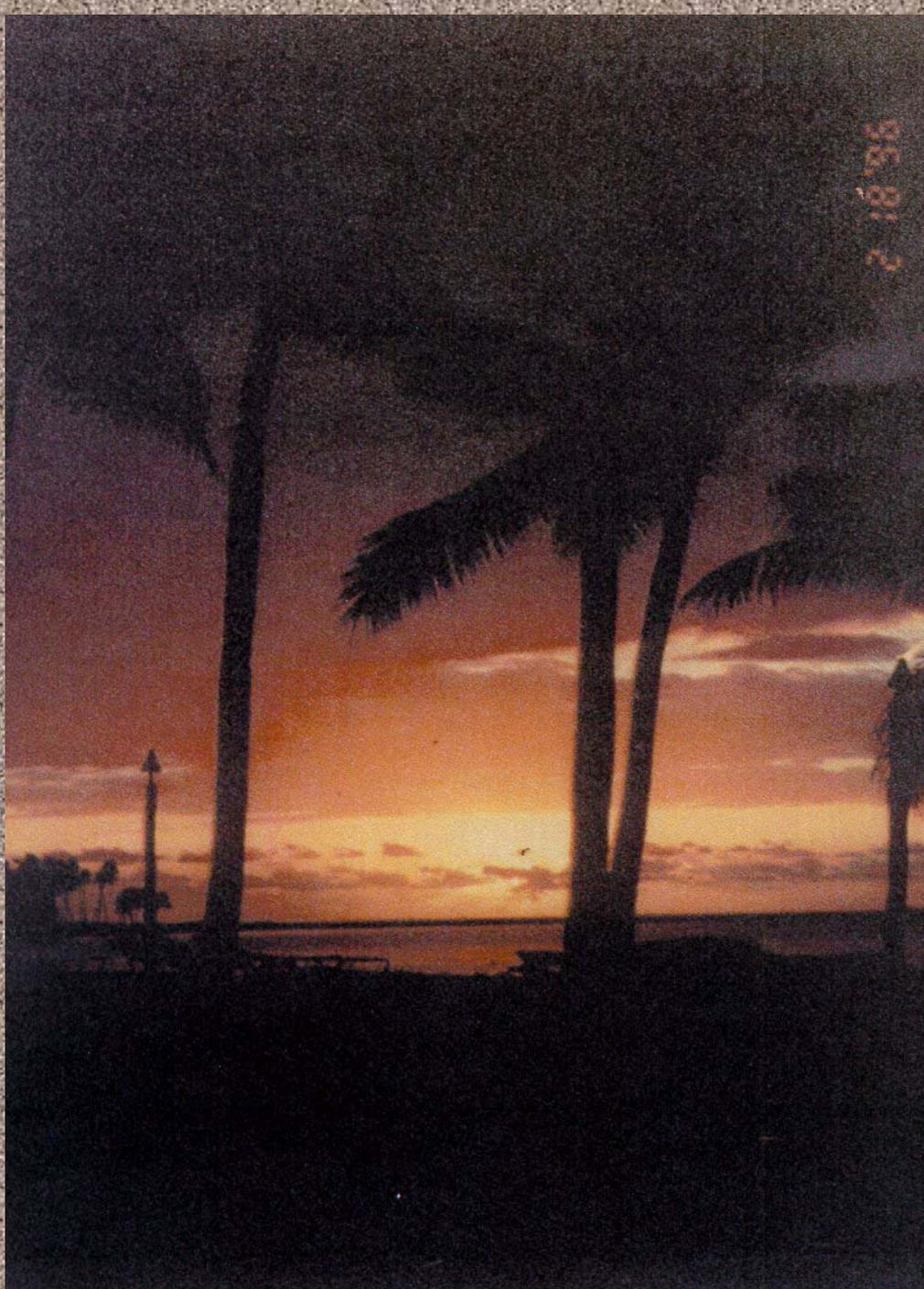
- **No design** "Just build a swamp here, fill that pond over there with manure and call it good."
- **Poor design** Undersized for load, applying wrong geochemical approach, phased design lacking, complex geochemistry, startup and operational procedures.
- **Not enough maintenance** (low maintenance does not mean "NO" maintenance).
- **Last minute changes** to construction specs can affect system performance - **experience helps.**

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- ARD Geochemistry (cell sequencing & cell type)
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In Water
Treatment, If
You're Not Part
of the **Solution**,
You're Part of
the **Precipitate**.

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